

STEAM METHANE REFORMING (SMR) FOR HYDROGEN PRODUCTION											
Date of factsheet	29-7-2018										
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Sector	Hydrogen										
ETS / Non-ETS	ETS										
Type of Technology	SMR-based hydrogen production without CCS										
Description	<p>Steam methane reforming (SMR) is a method that can be used for producing hydrogen from natural gas. This is achieved in a processing device called a reformer which reacts steam at high temperature with the gas. SMR uses the endothermic reaction</p> $\text{CH}_4 + \text{H}_2\text{O} \rightleftharpoons \text{CO} + 3\text{H}_2.$										
TRL level 2020	TRL 9 IEA (2017) reports 100.000 Nm <sup>3</sup> /h. at 10,8 MJ/Nm <sup>3</sup> , this translates to a capacity of precisely 300 MW hydrogen energy output. Progress ratio is found in Thomas (2009)										
TECHNICAL DIMENSIONS											
Capacity	Functional Unit		Value and Range								
	MW		300.00								
Potential	MW	NL	unlimited								
Market share	%		-								
Capacity utilization factor			1.00								
Unit of Activity	PJ/year										
Technical lifetime (years)	25.00										
Full-load running hours per year	8,322.00										
Progress ratio	0.95										
Hourly profile	No										
Explanation	IEA (2017) reports 100.000 Nm <sup>3</sup> /h. at 10,8 MJ/Nm <sup>3</sup> , this translates to a capacity of precisely 300 MW hydrogen energy output. Progress ratio is found in Thomas (2009)										
COSTS											
Year of Euro	2015										
Investment costs per year	Euro per Functional Unit		Current			2030			2050		
	mln. € / MW		0.74			0.74			0.74		
Other costs per year	mln. € / MW		-			-			-		
Fixed operational costs per year (excl. fuel costs)	mln. € / MW		0.03			0.03			0.03		
Variable costs per year	mln. € / MW		0.24			0.24			0.24		
Costs explanation	Data in NTNU(2016) is based on a different size plant, and the numbers here are scaled to represent the same size plant as in IEA (2017). All costs excluding fuel costs. Sinnott(2009) finds a higher (per kg H <sub>2</sub> output) value for investment costs, which can at least in part be explained by the use of data for a smaller size plant. In these figures, the OPEX costs amount to 3,6 % of the CAPEX costs. Conventional plants (such as SMR) benefit from economy of scale, so you can use a scale-up factor of 0.8 [Sinnott et al., 2009] when estimating the cost of a larger scale plant. All values based on LHV. Variable costs include here raw water make-up, catalysts and chemicals. Cost developments are taken relative to base year, and are found in Vita (2018). Cost for CO <sub>2</sub> capture are included.										
ENERGY IN- AND OUTPUTS											
Energy carriers (per unit of main output)	Energy carrier	Unit	Current			2030			2050		
	Main output: Hydrogen	PJ	-1.00			-1.00			-1.00		
	Electricity	PJ	-0.03			-0.03			-0.03		
	Natural gas resource (gas fields)	PJ	1.42			1.42			1.42		
		PJ	-			-			-		
Energy in- and Outputs explanation	Production of hydrogen; 10 <sup>5</sup> Nm <sup>3</sup> /h give 10,8*10 <sup>5</sup> *24*365*0,95 MJ = 8,99 PJ/y. The 0,95 factor is to account for active running hours per year. Other numbers are taken from IEA (2017) and NTNU (2016) and scaled accordingly. The NTNU study reports on a energy efficiency of 0,82, but based on their own reported values of in,- and outlet I find an energy efficiency of 0,96. A plant with an average power of 300*0,95 MW gives 8,99 PJ/year, and so all numbers are scaled by 8,99 to give a per PJ result. The 0.95 factor accounts for the utilization rate.										
MATERIAL FLOWS (OPTIONAL)											
Material flows	Material	Unit	Current			2030			2050		
			-			-			-		
Material flows explanation											

EMISSIONS (Non-fuel/energy-related emissions or emissions reductions (e.g. CCS))											
Emissions	Substance	Unit	Current			2030			2050		
	CO2	Mton	-	-	-	-	-	-	-	-	-
			-	-	-	-	-	-	-	-	-
			-	-	-	-	-	-	-	-	-
			Min	-	Max	Min	-	Max	Min	-	Max
			-	-	-	-	-	-	-	-	-
			Min	-	Max	Min	-	Max	Min	-	Max
		-	-	-	-	-	-	-	-	-	
		Min	-	Max	Min	-	Max	Min	-	Max	
Emissions explanation	These emissions are calculated by Opera from the fuel input, and therefore considered zero for this input field.										
OTHER											
Other			Current			2030			2050		
			-	-	-	-	-	-	-	-	-
			Min	-	Max	Min	-	Max	Min	-	Max
REFERENCES AND SOURCES											
IEA (2017). Techno-Economic Evaluation of SMR Based Standalone (Merchant) Hydrogen Plant with CCS. Accessed through <a href="https://ieaghg.org/exco_docs/2017-02.pdf">https://ieaghg.org/exco_docs/2017-02.pdf</a>											
Jakobsen, D. & Åtland, V. (2016). Concepts for large scale hydrogen production. Thesis, NTNU.											
Voldsund, M., Jordal, K. & Anantharaman, R. (2016). Hydrogen production with CO2 capture. International Journal of Hydrogen Energy, 41(9), 4969-4992.											
Expert opinion, Jacob Moulijn											
Sinnott, R.K. & Towler, G. (2009). Chemical engineering design: SI Edition. Elsevier.											
Ramsden, T., Steward, D., & Zuboy, J. (2009). Analyzing the Levelized cost of Centralized and Distributed Hydrogen Production Using the H2A production Model, Version 2 National Renewable Energy Laboratory, Virginia, 2009											
IEA (2015). Technology Roadmap - Hydrogen and Fuel Cells, OECD/IEA, 2015.											
Whitesides, R.W. (2005). Process equipment cost estimating by ratio and proportion. Course notes, PDH Course G 127.											
Vita, A. et al (2018). Sectoral integration- long-term perspective in the EU Energy System. ASSET											
Thomas (2009). Low-Cost Hydrogen Distributed Production System Development											